

IN THE SPECIFICATION:

Please replace the paragraph beginning at page 12, line 11, with the following rewritten paragraph:

- The mixture of coal/coke fines is cleaned and blended with tar or other fixed-carbon producing binders. The mix may then be formed into appropriate solid shapes. These shapes are then fed to a pyrolyzer, where the temperature is raised to 800-1100°C to devolatilize the solid objects driving off tars and gases and leaving a strong, high carbon-content coke. The gases and tars are cooled to approximately 300°C, condensing the tars, allowing them to be separated from the fuel-rich gas and collected. The tars are then recycled to be used within the process as a binder while the gases are oxidized to provide heat to the pyrolyzer. Calculations indicate that, with, for example only, a mix of 55% coke fines, 30% bituminous coal fines and 15% binder, the amounts of tars and gases generated are appropriate to operate the process in a closed-loop fashion. Of course these proportions will vary under control of one skilled in the art, depending on feedstock properties. At a briquette pyrolysis temperature of 900°C, typical product yields for the various constituents are shown in TABLE 2, below: -

Please replace the paragraph beginning at page 18, line 5, with the following rewritten paragraph:

B2 - An FMC formed coke plant, as stated above, uses multiple fluidized beds for char production and a curing oven and calciner for coke production. The processing and capital costs associated with commercial use of the present technology are expected to be much lower than for prior form coke processes, since the char production step is eliminated. Total costs for coke production from the present process are likely to be in the range of \$50-60/ton, without requiring the sale of by-products. Current metallurgical coke prices are in the range of \$100-120/ton and foundry coke is \$140-160/ton. -